

Challenges in Modeling Complex EV Thermal Management Systems

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Table of Contents

- Component Modeling
 - General Best Practices
 - Evaporators & Condensers
 - Plate Heat Exchangers
 - Compressors
 - Expansion Valves
 - Ducts & Tubes

- System Modeling
 - Parameter Variation & Optimization Targets
 - Subsequent Operating Points



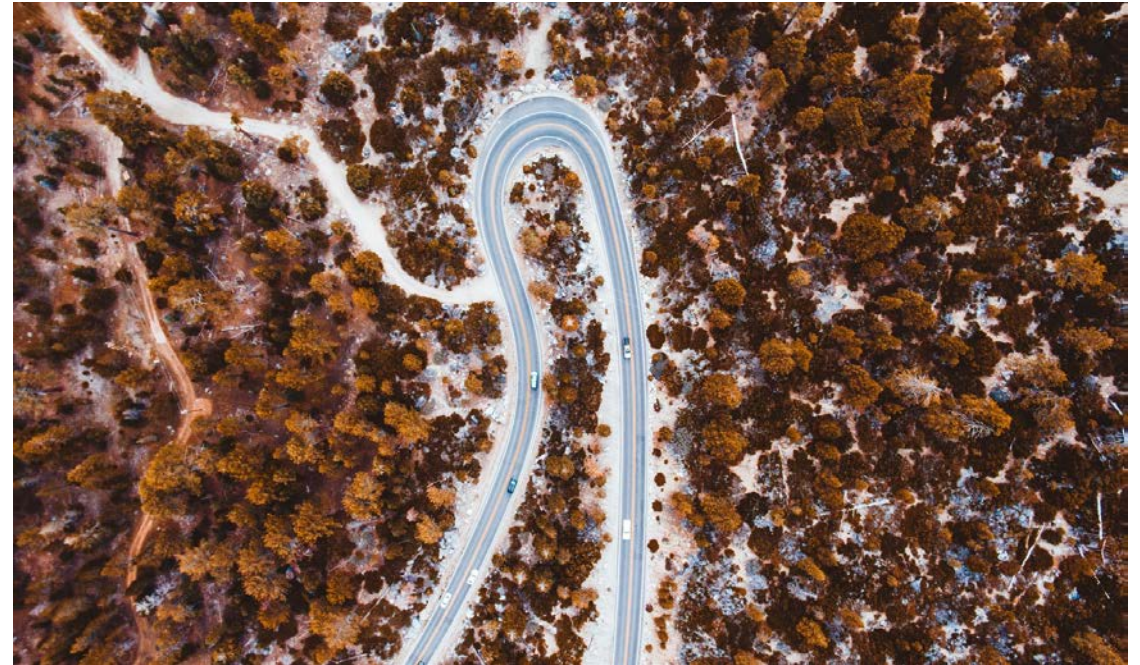
Component Modeling



General Best Practices

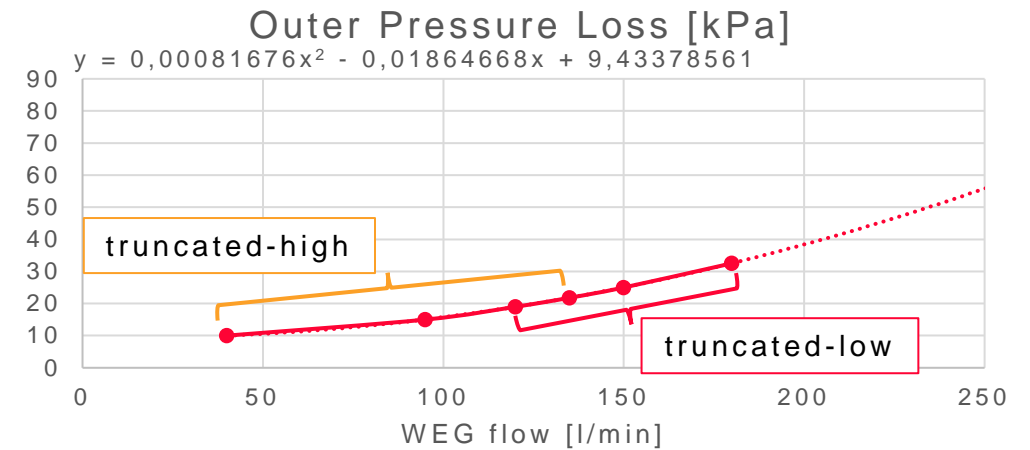
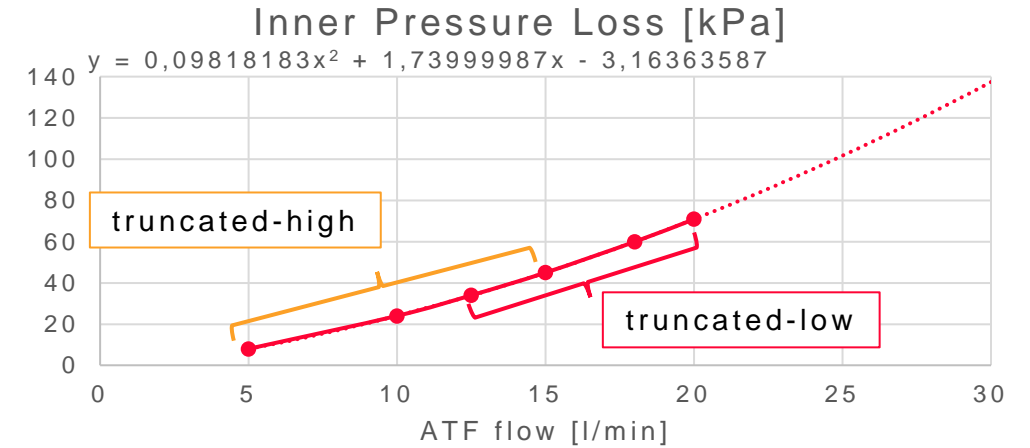
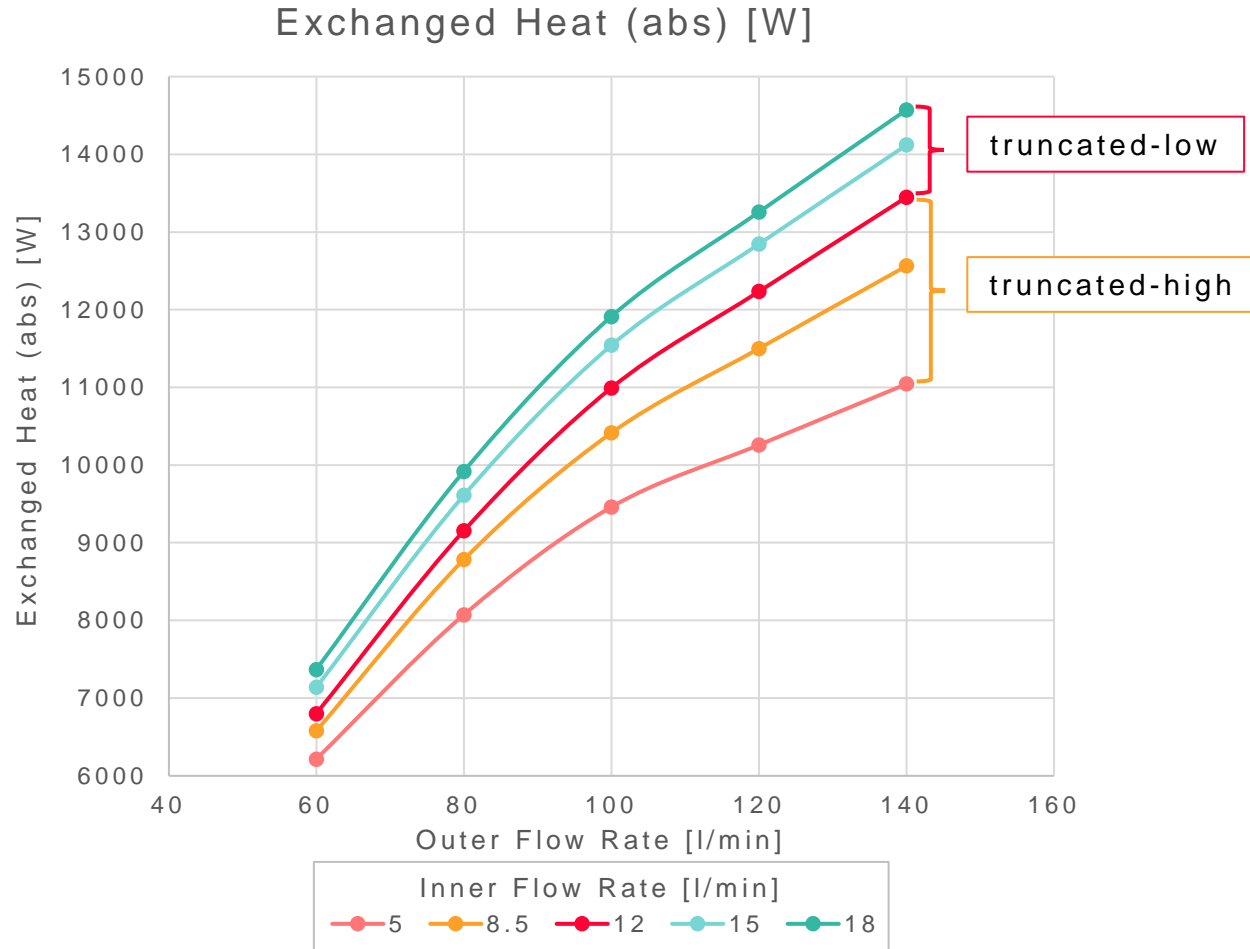
HOW TO HANDLE COMPONENT DATA

- Extrapolating more than 5-10% is not advised.
- Interpolating is usually not a problem -- cover your desired range and you'll be fine.
- When the operating range is large, you may calibrate for high volume and low volume flow ranges separately
 - This approach results in 2 component files...
 - ...but results are better and solve faster!
- It is important to always do some inspection of all component data before we use it in a model. Bad data will cause bad results at best, or no results at worst.
- Always check the data!



Effects of Extrapolation - Inputs

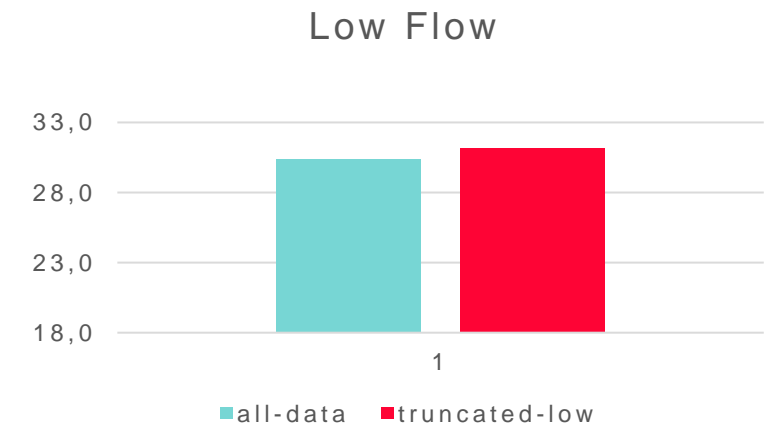
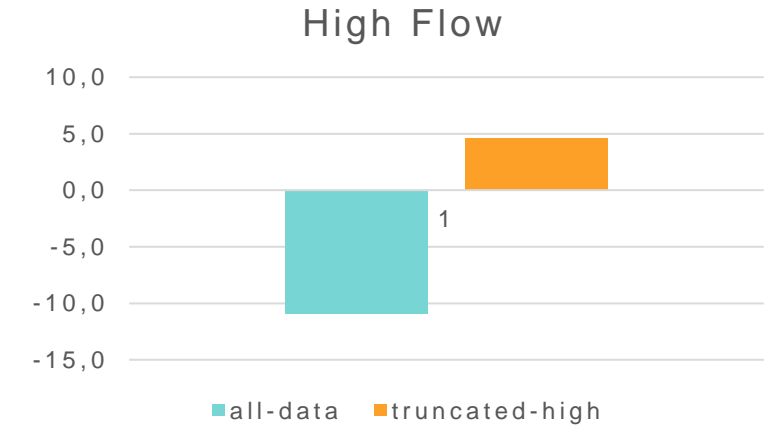
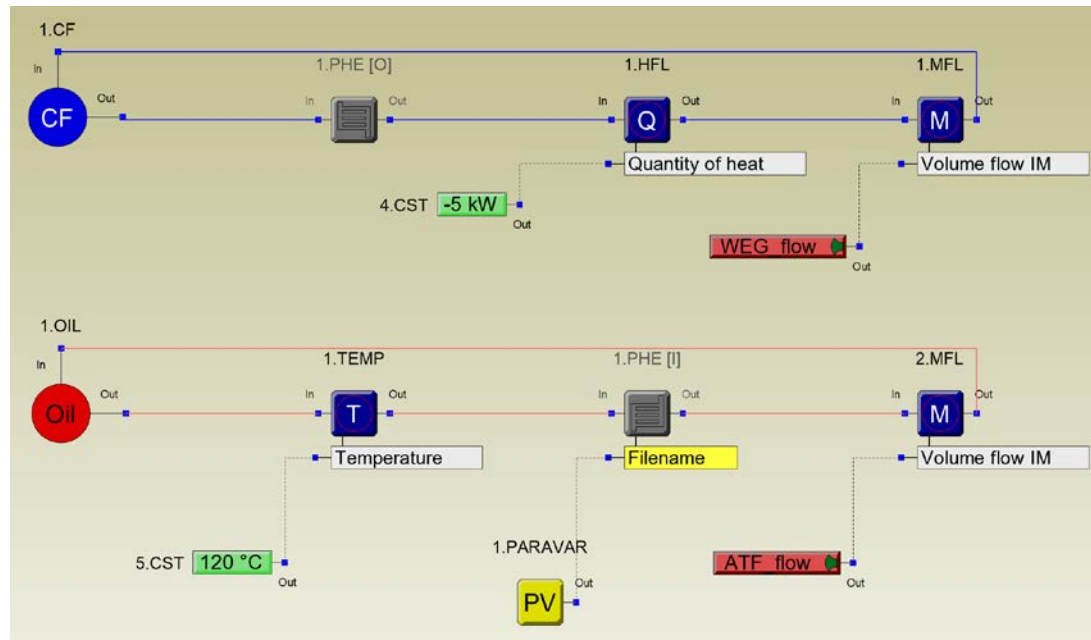
A PLATE HEAT EXCHANGER, A COMMON COMPONENT IN EV THERMAL SYSTEMS



Effects of Extrapolation – Model & Outputs

A PLATE HEAT EXCHANGER, A COMMON COMPONENT IN EV THERMAL SYSTEMS

- Testbench model shown below
- Results shown at right
- Effects of extrapolation are more pronounced at higher flows!



Evaporators & Condensers

THE HIGH AND LOW OF REFRIGERANT CIRCUITS

- Why calibrate and check errors?
- The goal is to get the component model to behave the same way as the measurement data
- In most cases, calibration works well if the input the geometry is accurate
- If calibration fails or produces large errors, we **must** inspect the input data!



Evaporators & Condensers

A COMPONENT DATA VETTING PROCESS

Compare geometric properties with a known-good component

If something looks odd, consult the drawing and recalculate it manually

If there is no drawing available, adjust incrementally and recalibrate & recheck errors

When errors are low, stop. If not, continue incremental adjustments then rinse & repeat

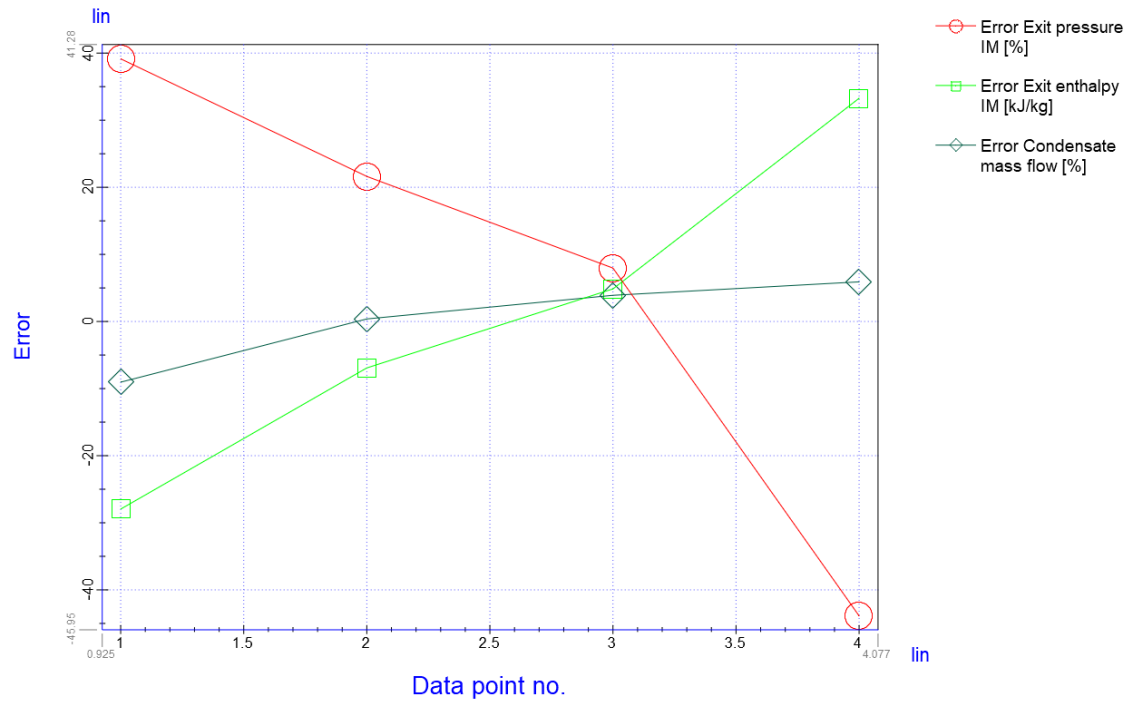
Always try to keep as much original data as possible!



Evaporators & Condensers

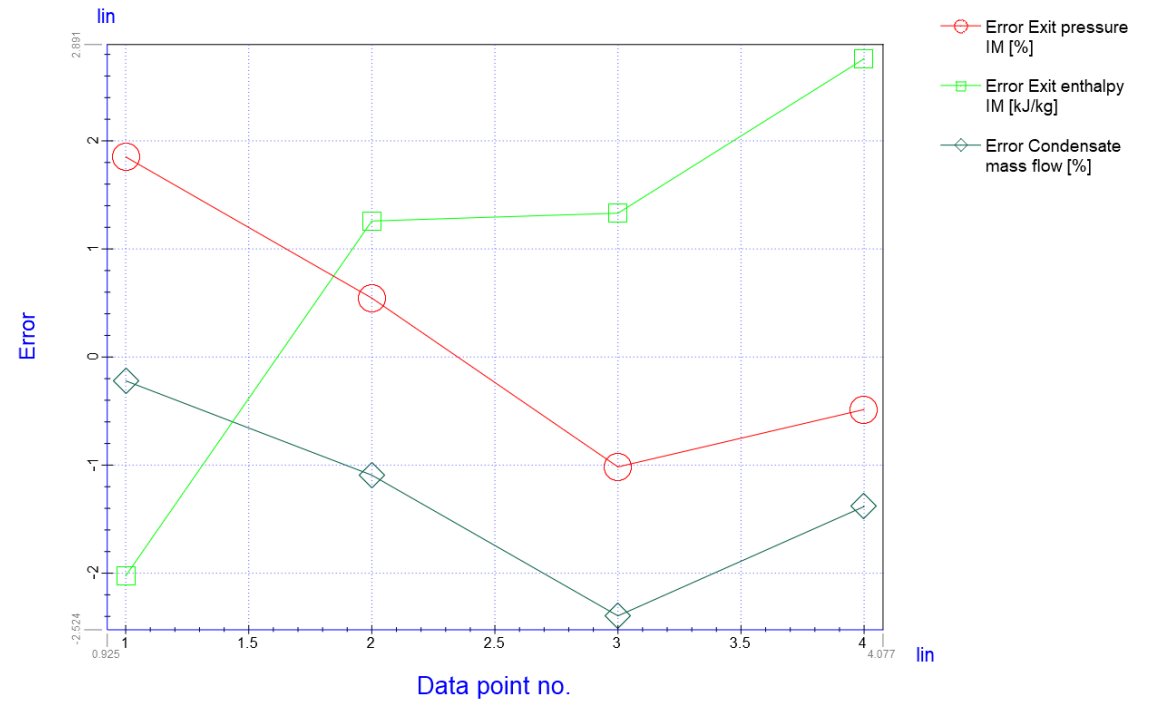
A WHO'S WHO OF THE GOOD AND THE BAD

Evaporator: Error Measurement - Simulation



BAD

Evaporator: Error Measurement - Simulation



GOOD

Evaporators & Condensers

A FEW USUAL SUSPECTS

- Usually, geometry is the cause of high errors and calibration failure
 - Fin pitch and thickness airside (0.3mm is a good guess)
 - Distance between tubes
 - Tube height and wall thickness (0.4mm is a good guess)
- If you can't get a drawing, get a part and start cutting!
- Other areas to check:
 - End tank volume, ensure cross section and core dimensions add up to the specified volume
 - Refrigerant enthalpy can be checked using KULI's property calculator
 - Plot points on the P-h diagram as a sanity check
- The difference between a pipe and a tube is frequently misunderstood. Make sure the input data was provided with the correct understanding in mind.

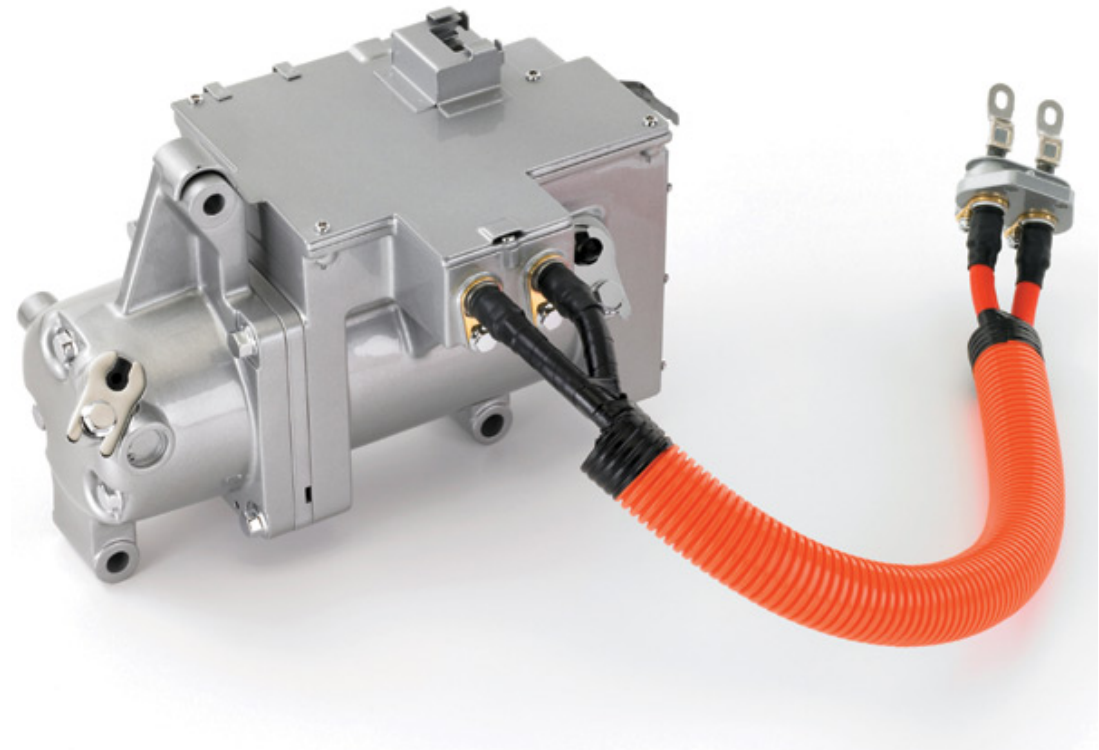


Compressors

GETTING TO THE HEART OF THE MATTER

- E-Compressor performance data should follow positive-displacement device trends:
 - Low-speed efficiency suffers due to rotor leakage
 - High-speed efficiency suffers from dynamic filling effects
 - Best efficiency is usually somewhere in the middle
- If the curves follow a different trend, find out why!
- Input power is essential for EV range prediction, but often only efficiency is provided. Use the polytropic compressor power equation to define ideal input power:

$$P = \left(\frac{n}{n-1} \right) \cdot P_s \cdot V_d \cdot \left(\frac{N}{60} \right) \cdot \left(\left(\frac{P_d}{P_s} \right)^{\frac{n-1}{n}} - 1 \right)$$

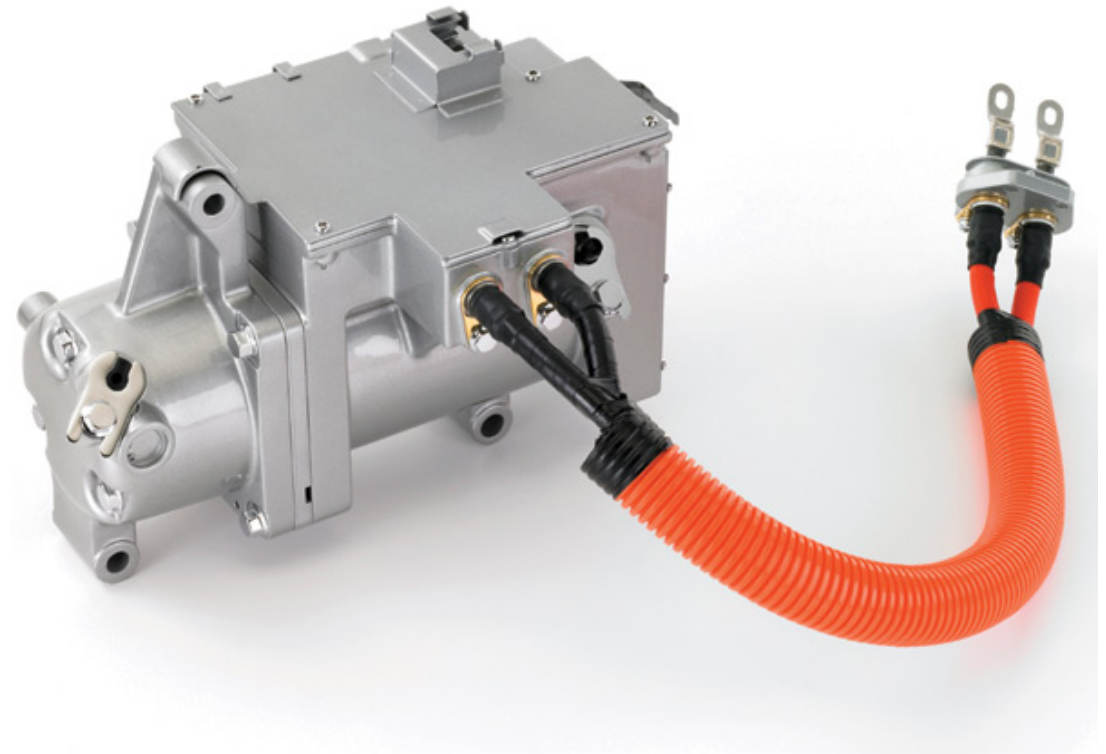


GM, DaimlerChrysler and BMW Two-Mode Hybrid Electric AC Compressor

Compressors

IT'S A SPEED THING

- It is tempting to use an optimization target to find the compressor speed that corresponds to a temperature target
- In practice this does not work very well!
- It is *usually* faster to set the compressor speed to a constant value and adjust it manually



GM, DaimlerChrysler and BMW Two-Mode Hybrid
Electric AC Compressor

Plate Heat Exchangers

DYNAMIC SOLVER WORKAROUNDS

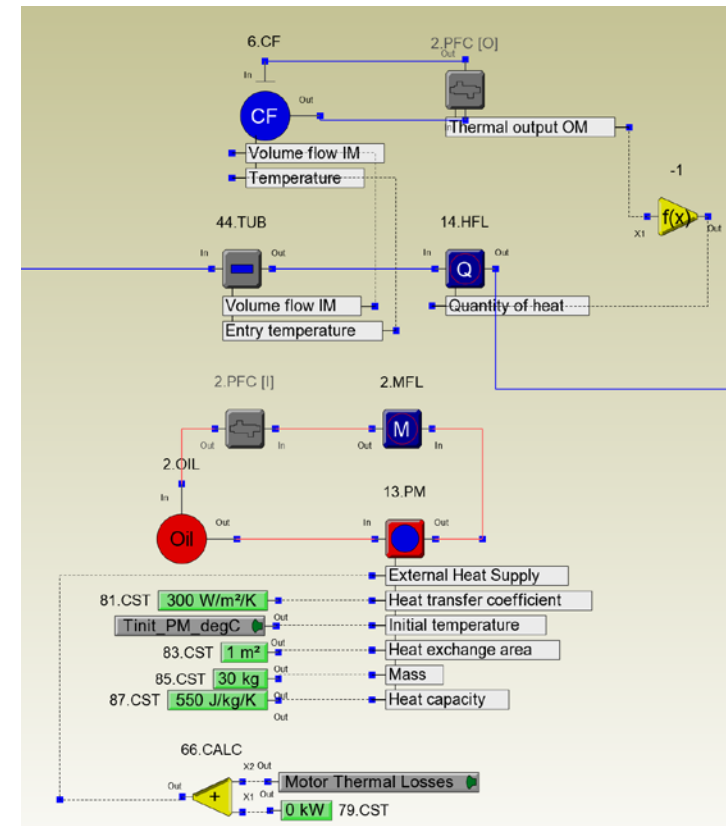
- EV thermal systems typically have operational modes in which no coolant flows:
 - Warmup events
 - “Idling”
 - Powertrain during charging
- To model zero-flow modes, the dynamic solver must be enabled...
- But the dynamic solver isn’t permitted with plate heat exchangers. What to do?



Plate Heat Exchangers

DYNAMIC SOLVER WORKAROUNDS

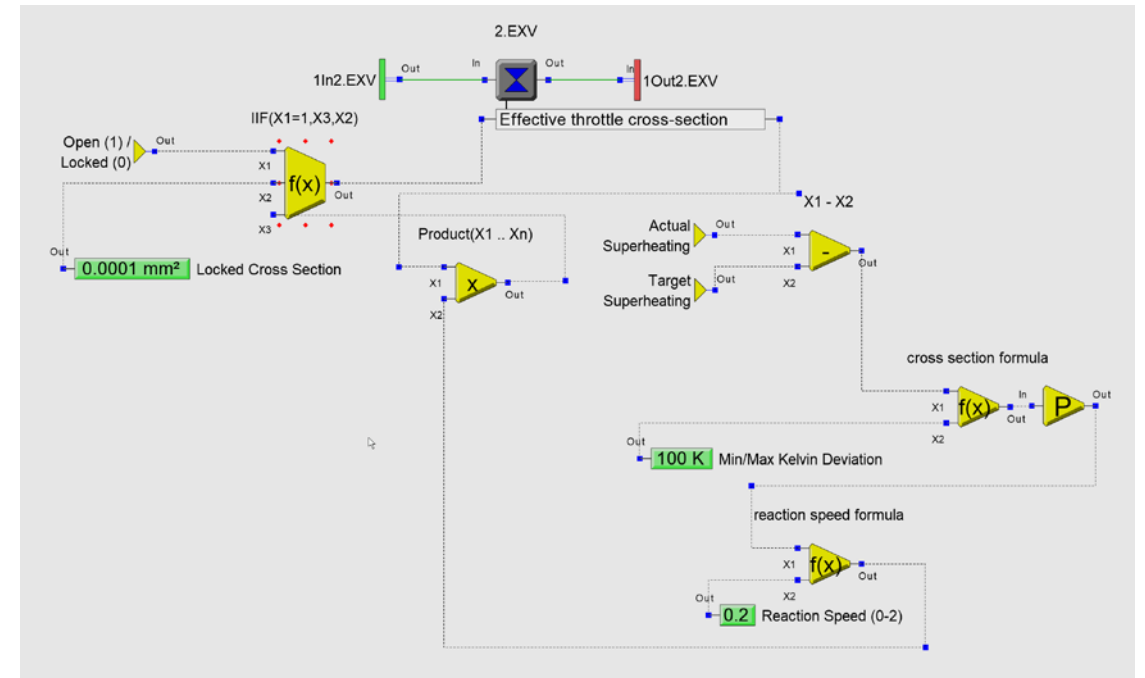
- An example workaround is shown at right using a parallel flow cooler, technique is the same with a plate heat exchanger
- The pressure drop and heat transfer of the heat exchanger are implemented with a tube and a heat flow source, which are allowed in dynamic solver circuits
- The values for pressure drop heat transfer are calculated in a dummy circuit that uses the standard solver
- Dummy circuit values are passed to the dynamic solver via sensors and actuators, using formulas where appropriate



Expansion Valves

TO SHUT OFF OR TO GO WITH THE FLOW

- EV thermal systems commonly contain multiple expansion devices:
 - Coolant chiller
 - Evaporators
- If multiple thermal expansion valves are used, this will cause system instability. What to do?
- Shown at right is an implementation of a TXV with shutoff
- The effective throttle cross section is controlled using a series of formulas:
 - Superheat error is translated into an area, passed to the valve with an actuator
 - Valve can be shut off using a logical operator



Ducts & Tubes

HEAT ON THE PATH OF SOME RESISTANCE

- Minimizing pressure loss in ducts is common design goal when developing a cabin HVAC system. But what about the heat transfer *into* the duct from its environment?
- Heat transfer in ducts can be modeled in two ways:
 - using point masses and conduction paths
 - using a heat source in the airpath
- Blowers tend to operate as constant mass-flow devices in cabin HVAC systems
- As a rule of thumb, heat transfer into ducts from ambient has a greater effect on outputs like cabin temperature than pressure drop inside ducts
- Tubes can be modeled using only 2 points, but results are often unreliable due to excessive interpolation
- 3 points are better, parametric equations are *best!*



System Modeling

Parameter Variation & Optimization Targets

GOLDBLOCKS IS BACK AND FORTH AND BACK AGAIN

- Running parameter variations or optimization targets in refrigerant loops is not straightforward
- If one point doesn't solve then you are waiting for a long time for no results, not knowing where the problem is!
- Restricting the range of variation can help sometimes
- Manual variation is *usually* best



Subsequent Operating Points

FIRST THIS, NOW THIS

- The KULI solver initializes the refrigerant loop with default values
- When the first operating point finishes, the solver initializes the second operating point at the state in which the first point solved
- If this state is too far off of the solution for the second point, the solver may fail or produce an unrealistic result
- To avoid this problem:
 - Make small incremental changes in simulation parameters for subsequent operating points
 - Limit the number of parameters that change from one point to the next to one or two at most



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Questions?

A STARTING POINT

- What should I look for when using the KULI refrigerant property calculator to verify evaporator and condenser calibration?
 - On P-h diagram plots:
 - Evaporator inlet should be under the dome
 - Condenser inlet should be to the right of the dome
- When using the polytropic compressor power equation to define ideal input power, what is an appropriate value for n , the polytropic expansion coefficient?
 - For r134a, $n = 1.08 - 1.10$
- Does a tube have fins?
 - NO!
 - **Remember:** *Pipes go inside tubes, fins go inside pipes*



Thank You

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