

## Coupling MATLAB with KULT for ORC System Optimisation

G Yu

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### **Backgrounds & Objectives**

- An organic Rankine cycle (ORC) test rig was designed and being constructed in DENSO Marston Ltd for test of phase change heat exchangers, such as boilers and condensers, used in ORC systems for heavy duty off-highway vehicles.
- To operate this complex system to meet customer specs is not possible through trial and error for example for an operating condition with 6 variables.
- The requested test working conditions can be identified by KULI's optimisation process.
- It was found that KULI optimiser is too sensitive to the bound values of design parameters therefore can not always find the optimal solutions. A professional optimiser was recommended for this purpose.
- A method was developed to couple KULI with MATLAB's optimisation algorithm as an alternative.



### **Brief Introduction of the ORC System Test Rig**







Rig under construction

#### System information:

- Organic fluid: R1233ZD
- Evaporation pressure: 26.3 bar
- Condensation pressure: 6.6 bar
- Hot air as heating source for evaporator
- Ambient air as cooling sink for condenser

#### System processes & components

- Pump (A->B)
- Electric heater + Recuperator (B->C)
- Evaporator (C->D)
- Expansion valve + water cooled cooler (D->E)
- Recuperator (E->F)
- Condenser + Storage tank with electric heater + Water cooled cooler (F->A)

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### **System Diagram for Tail Pipe Boiler Test**



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### **System Simulation - Tail Pipe Boiler Test**



#### Design Targets

- 1. Boiler entry sub cool (K)
- 2. Boiler exit super heat (K)
- 3. Condenser entry super heat (K)
- 4. Condenser exit sub cool (K)
- 5. Storage tank sub cool (K)
- 6. Pump entry sub cool (K)

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#### **Design Parameters**

- A. Refrigerant mass flow rate (kg/min)
- B. EGR emulator (modelled by elec. Heater) power input (kW)
- C. Water mass flow rate post expansion cooler circuit (kg/s)
- D. Cooling air velocity (m/s)
- E. Storage tank electric power input (kW)
- F. Water mass flow rate pre-pump cooler circuit (kg/s)

### Why Coupling MATLAB with KULI

When building the KULI evaporator component, if the input data covers a wider range, its discontinuity from non-phase to phase change or vice versa may lead to the KULI model failing to find the optimal solutions as shown below:



#### Design Parameters Values

7.OPTPAR: 50072.0395 6.OPTPAR: 0.177032941 5.OPTPAR: 4661.02082 3.OPTPAR: 4.8092379 2.OPTPAR: 0.696466886 1.OPTPAR: 0.885145751

#### **KULI** Optimisation Results

OP 1: 1.Expansion device - is working in mixed phase area! Opt. target 1.TUB: Subcooling temperature IM: 20.0741015 [K] Opt. target 4.ACPHE: Subcooling temperature IM: 3.37829305 [K] Opt. target 2.TUB: Subcooling temperature IM: -4.97219476 [K] Opt. target 2.CND: Subcooling temperature IM: 1.27063308 [K] Opt. target 2.EVP: Superheating temperature IM: -35.1139483 [K] Opt. target 2.ACPHE: Superheating temperature IM: -14.8099924 [K]





Solution: KULI for system simulation only, optimisation process by MATLAB

### A Simple KULI System for Feasibility Study



- Two variables to be optimised
  - 1.coolant circuit heat input *radiatorQ* (kW)
  - 2.fan speed fanSpeed (1/min)
- Two targets to be achieved
  - 1.Radiator coolant entry temperature 98 Deg C
  - 2.Charge air exit temperature 35 Deg C

### A Simple KULI System – Setup in MATLAB



### A Simple KULI System – Comparison Between MATLAB & KULI Optimisation



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### **ORC System Optimisation - MATLAB**

#### KULI file name = ORC tail pipe boiler test for MATLAB.scs





### **ORC System Optimisation - MATLAB**

```
function targets = callkuli(parameters)
                                                                                   KULT HVAC
⊢€
       global kuli
                                                                                   KULI AC: Maximum number of circuit equalizations in overall system
                                                                                                                                                              400
 읗
       For KULI v13 and later
 <del>s</del>
       kuli = actxserver('KuliAnalysisServer.KuliAnalysisCtr2.13.1');
                                                                                   KULI AC: Truncation condition for enthalpy equalization [%/100]
                                                                                                                                                              0.001
 - 8
       For other earlier KULI versions
                                                                                   KULI AC: Truncation condition for subcooling/superheating equalization [K]
                                                                                                                                                              0.001
     kuli = actxserver('KuliAnalysis2.KuliAnalysisCtr2.12.x64');
       kuli.registerevent({'OnMessage', @kuliOnMessage; 'OnError', ...
 읗
                                                                                                                                         0.1 before
           @kuliOnError});
     fileName = ...
                                                                                     % Define design parameter lower/upper bounds
         'D:\ORC tail pipe boiler test for MATLAB.scs';
                                                                                     % 1.....refrig mass flow rate, kg/s [10, 75]/60
     kuli.set('KuliFileName', fileName);
                                                                                     % 2.....preheater power, kW [0.1, 100]
     kuli.invoke('Initialize');
                                                                                     % 3.....tank heater power, kW [0.01, 10]
                                                                                     % 4.....postExp flow rate. kg/s [0.01, 1.5]
     kuli.invoke('SetCOMValueByID', 'refrig mass flow rate', parameters(1));
                                                                                     % 5.....prePump flow rate, kg/s [0.01, 0.2]
     kuli.invoke('SetCOMValueByID', 'preheater power', parameters(2));
                                                                                     % 6.....air on vel, m/s [1, 10]
     kuli.invoke('SetCOMValueByID', 'tank heater power', parameters(3));
                                                                                     % order important
     kuli.invoke('SetCOMValueByID', 'postExp flow rate', parameters(4));
     kuli.invoke('SetCOMValueByID', 'prePump flow rate', parameters(5));
                                                                                     number of variables = 6;
     kuli.invoke('SetCOMValueByID', 'air_on_vel', parameters(6));
       kuli.invoke('RunAnalysis');
                                                                                     % ObjectiveFunc = @objectiveFunction; %dummy objective function
     kuli.invoke('SimulateOperatingPoint', int8(1));
                                                                                     Constraints = @constraints;%define constraints for optimiser
                                                                                     ConstraintTolerance Data = 1e-4; %1e-4;%set constraint tolerance
     targets(1) = kuli.invoke('GetCOMValueByID','eva subcool');
                                                                                     StepTolerance Data = 1e-6;% X step size tolerance
     targets(2) = kuli.invoke('GetCOMValueByID', 'eva superheat');
                                                                                     FiniteDifferenceStepSize Data = [0.01, 0.01, 0.01, 0.01, 0.01, 0.01];
     targets(3) = kuli.invoke('GetCOMValueBvID','con superheat');
     targets(4) = kuli.invoke('GetCOMValueByID', 'con subcool');
                                                                                     LB = [10/60, 0.1, 0.01, 0.01, 0.01, 1];
     targets(5) = kuli.invoke('GetCOMValueByID','tank subcool');
                                                                                     UB = [75/60, 100, 10, 1.5, 0.2, 10];
     targets(6) = kuli.invoke('GetCOMValueByID', 'pump subcool');
                                                                                     % Define design parameter initial values
     kuli.invoke('CleanUp');
     kuli.delete;
                                                                                     x0 = ones(1, number of variables);
 end
                                                                                   for i=1:number of variables
                                                                                         x0(i) = 0.5* (LB(i) + UB(i));
                refrig mass flow rate [kg/s]
                                              eva_subcool [K]
                                                                                     end
                                     nthy of heat
                                                                                     % Call MATLAB 'fmincon' optimisation algorithm to
           prePump flow rate (kp/s)
                                                               eva_superheat [K]
                                                                                     % Find a minimum of a constrained nonlinear multivariable function
                                                                                     [x,fval,exitflag,output] = fmincon opt(@(x)0, x0, LB, UB, ...
                                                                                         Constraints, ConstraintTolerance Data, StepTolerance Data, ...
                                                                                         FiniteDifferenceStepSize Data);
                                                                                     % Final run to get the targets
                                                                                     v = callkuli(x);
                        temperature IM
                                                                                     disp(output);
        pun p_subcool (K)
                         tank_subcool (K) tank_heater_power (KW) Sub
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                                                                                                                                                       11/**
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```

### **Bound Sensitivity Analysis - MATLAB & KULI**

Design Parameters E			Βοι	Bound-1		Bound-2		Bound-3			
1. Refrigerant mass flow rate (kg/min)			10	~ 75	20~37.5			10 ~ 75			
2. EGR emulator (modelled by elec. Heater) power (input (kW)			0.1	~ 100	0.2 ~ 66.67		1~400				
3. Storage tank electric power	input (kW	)	0.0	1~10	0.0	)2 ~ 5		1 ~ 200			
4. Water mass flow rate – post expansion cooler circuit (kg/s)				1~1.5	0.02 ~ 0.75			0.01 ~ 10			
5. Water mass flow rate – pre-pump cooler circuit (kg/s)			0.0	1~0.2	0.05 ~ 0.2			0.01 ~ 5			
6. Cooling air velocity (m/s)			1~	10	2~ 10			1~10			
						KULI+M	AT	LAB			
Design Targets	Targets	Values – Bound 1		%		Values – Bound 2	%	•	Value Boun	es – d 3	%
1. Evaporator entry sub cool (K)	3	2.97		99%		3.026	1(	01%	3.003	34	100%
2. Evaporator exit super heat (K)	5	5.03		101%		4.98	1(	00%	5.003	33	100%
3. Condenser entry super heat (K)	3.6	3.63		101%		3.58	9	9%	3.600	)7	100%
4. Condenser exit sub cool (K)	3	3.01		100%		3	1(	00%	3.018	39	101%
5. Storage tank sub cool (K)	0.05	0.0626		125%		0.0526	1(	05%	0.068	36	137%
6. Pump entry sub cool (K)	5	5.01		100%		5.0029	1(	00%	4.976	56	100%

		KULI									
Design Targets	Targets	Values – Bound 1	%	Values – Bound 2	%	Values – Bound 3	%				
1. Evaporator entry sub cool (K)	3	2.93	98%	2.894	96%	2.711	90%				
2. Evaporator exit super heat (K)	5	4.95	99%	5.231	105%	7.099	142%				
3. Condenser entry super heat (K)	3.6	3.678	102%	3.769	105%	-0.172	-5%				
4. Condenser exit sub cool (K)	3	2.953	98%	3.003	100%	4.251	142%				
5. Storage tank sub cool (K)	0.05	0.005	10%	0.0505	101%	-0.399	-798%				
6. Pump entry sub cool (K)	5	4.959	99%	4.996	100%	5.669	113%				

- Bound-1 initial guess
- Bound-2 improved one based on optimal results from Bound-1, much closer to the optimal results
- Bound-3 mixed between Bound-1 & Bound-2 for algorithm robustness check

- MATLAB has a better consistence
- MATLAB is more flexible, which allows users to set up problem dependent simulation controls to achieve a better solution
- Both can not deal with Design target 5 except for Bound-2, i.e. the bound range is narrower around the true solution
- Compared with KULI, MATLAB takes a longer but affordable simulation time, ~45 minutes on a desktop with 3.06GHz CPU, 48GB RAM, 64 bit system

### Conclusions

- KULI optimiser worked well when design parameter bound values were narrow enough around true optimal solutions.
- A method was developed to use KULI for system simulation, MATLAB optimisation algorithm for optimisation process.
- An ORC system with 6 design parameters and 6 design targets was successfully optimised using KULI coupled with MATLAB.
- Bound sensitivity analysis showed that KULI optimiser was more sensitive to the bound values, KULI/MATLAB was more flexible and robust.
- It was also shown that compared with KULI, KULI/MATLAB took a longer but affordable simulation time.
- Possible improvement of KULI optimiser to deal with phase change heat exchangers for ORC system optimisation?



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